

Microwave assisted multiwall carbon nanotubes enhancing Cd(II) adsorption capacity in aqueous media



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ABSTRACT

Novel multiwall carbon nanotubes (MWCNTs) have been successfully synthesized using tubular microwave chemical vapour deposition technique and proved to be an outstanding adsorbent for the removal of Cd(II) from aqueous solution. The effect of process parameters such as pH, MWCNTs dosage, agitation speed and time were investigated. The maximum adsorption capacities of Cd(II) were found to be 88.62 mg/g and a statistical analysis reveals that the optimum conditions for the highest removal (98%) of Cd(II) are at pH 5, MWCNTs dosage 0.1 g, agitation speed and time of 160 rpm and 50 min, respectively with the initial concentration of 10 mg/L. The Langmuir and Freundlich isotherm models match the experimental data very well and adsorption kinetic obeyed pseudo-second order. Our results proved that MWCNTs can be used as an effective Cd(II) adsorbent due to the high adsorption capacity as well as the short adsorption time needed to achieve equilibrium.

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Introduction

New era industries have immensely improved the living standard of human being. But however, these modern industries also pose serious adverse impacts on our living surrounding. One of the major environmental concerns is the water pollution by the heavy metals. Heavy metals in water are the main preoccupation for many years because of the toxicity towards aquatic-life, human beings and also the environment [1]. Even though trace amounts of heavy metals are vital for the human body, they are considered as harmful when they become excessive. Contrasting with organic pollutants, most of which are susceptible to biological degradation, heavy metal ions do not end product that is harmless to the environment. The contamination of crucial concern includes lead, cadmium, mercury, zinc, chromium, silver, Tin, and other

mutagenic nature which also makes up the earth's surface [2–6]. Contamination of heavy metals exists in aqueous wastes of various industries, such as mining operations, tanneries, metal plating, alloy industries and smelting [7]. A process involving industries such as metal plating and battery manufacturing can be counted as the primary source for cadmium pollution in water [8]. Cadmium is heavy metal ion which is vastly known as one of the toxic material which can be exposed to mankind either in the environment or at work. Due to the low rate of excretion of body, cadmium has a long biological half-life [9]. This explains why, if it is absorbed in one's body, cadmium remains there and accumulates throughout life. Primarily, Cadmium affects the kidney, specifically to the proximal tubular cell, main site of accumulation. Moreover, prolonged exposures to cadmium cause toxicity due to accession over time in various body tissues, including liver, chronic disorders like 'itai-itai' diseases, renal damages and emphysema [10,11]. The World Health Organization recommended the drinking water guideline value to be 0.005 mg Cd/L [12]. Cadmium and certain cadmium compounds are probable or suspected carcinogens, hence, it is compulsory to remove cadmium from drinking and waste waters.

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Various chemical removal methods have been utilized and also further developed over the decades to take charge of the heavy metal contaminations. Removal of heavy metal from aqueous solution consists of physical, chemical and biological techniques. Suggested conventional methods are electrochemical treatment, chemical precipitation, membrane technologies and adsorption on activated carbon [13]. Amongst all the methods, adsorption on activated carbon is considered to be very promising in terms of its efficiency of removal from aqueous solutions [14]. In addition, it is another good method to be taken into account from the aspect of handling methods and economics. Even though there are so many adsorbents available, researchers had to come up with a new adsorbent as the existing adsorbents were lacking in its efficiency to remove metal ions [15].

Carbon nanotubes (CNTs) are a new member in carbon family, essentially a new type of adsorbents that proves to retain great potential for removal of pollutants such as herbicides, chloro-benzenes, as well as lead and cadmium ions [11]. CNTs consist of a hollow and layered structure along with a large specific surface area [16] which leads to a remarkable application as an adsorbent with a high adsorption capacity for water treatment by utilizing the adsorption method. Hence, nanomaterial proves to be an essential adsorbent due to its high specific surface area along with efficient active sites for adsorption of Cd(II) from water. CNTs have a relatively larger specific area that provides a good opportunity for the removal of heavy metals [17–19]. Carbon based nanomaterial was opted to provide an alternative method for water treatment and few of these materials provided an astonishing outcome with a high rejection of contaminant from water. Carbon nanotubes based technologies found its water-treatment applications in various fields, for instance, as sorbents, catalyst, filters, or membranes [17]. It is of common interest that the development of a new technique for an efficient and the selective synthesis of carbon nanotubes at the cheapest possible cost [20]. One of such possibility is the use of microwave radiation. The reason behind the choice of microwave used to produce carbon nanotubes is the novelty of this method [21]. Microwave-assisted modification of carbon nanotube is non-invasive, simple, fast, environmentally friendly and clean method as compared to traditional methods. Usually, the use of the microwave facilitates and accelerates reactions, often improving relative yields [22]. The use of microwave radiation in the synthesis and functionalization of carbon nanotubes or other nanostructures is advantageous because it provides a fast and uniform heating rate that can be selectively directed towards a targeted area compared to the conventional method used. In our innovation microwave-assisted synthesis, including fast multiwall carbon nanotube (MWCNTs) growth and ambient reaction condition, lowers the cost, and simplifies the procedure leading to a high yield synthesis of high-quality MWCNTs with minimal impurity. Unlike conventional heating, microwave heating has a higher heating rate, which results from the intrinsic transition of electromagnetic energy to thermal energy by a molecular interaction with the electromagnetic field, rather than heat transfer by conduction or convection.

In this research, a novel MWCNTs was synthesized using tubular microwave chemical vapour deposition. The developed MWCNTs tested for Cd(II) adsorption capacity in aqueous media, also a statistical optimization of process parameters such pH, MWCNTs dosage and agitation speed and time of removal of Cd(II) were investigated. The studies on the isotherm kinetic and isotherm model were developed and investigated as well. The thermodynamic parameters and desorption studies were investigated as well.

Materials and methods

Experimental setup for MWCNTs production

The schematic of tubular microwave chemical vapor deposition (TM-CVD) for MWCNTs production as described in my previous work [23]. The horizontal tubular microwave model Synotherm-T1500, China reactor for production of MWCNTs. It comprised a quartz tube of 55 mm OD, 50 mm ID and 615 mm length. Ferrocene catalyst was placed at the entrance of the chamber and quartz boat size was placed at middle of the reaction chamber. The system was initially flushed with Ar in order to ensure an oxygen free environment. The gas flow rate of C₂H₂ and H₂ was free mixed before entering into the tubular microwave chamber using gas mixture Model KM-20-2, Germany, after the gas mixture was sent to microwave chamber. The reaction was carried on for the desired time period and on completion, the total amount of MWCNTs produced in the quartz boats was collected and weighed. The optimized conditions for the high weight of MWCNTs production was at 900 W microwave power, 35 min radiation time and 0.6 gas ratio of C₂H₂/H₂. The optimized produced MWCNTs have high BET 206 m²/g surface area having a particle size of 450 μm that leads to high efficiency in removal of Cd(II) from aqueous solution.

Preparation of stock solutions

Analytical grade Cd(II) standard solution which was obtained from Merck was used to prepare stock solutions containing 1000 mg/L of Cd(II) metal ions which were further diluted with distilled water to obtain the required concentrations. As for this research, the initial concentration of Cd(II) metal ions was set to 10 mg/L and the prepared solution were used for batch adsorption experiments.

Batch adsorption experiment

A batch adsorption experiment was performed by using 100 mL of 10.0 mg/L of Cd(II), agitated with varying dosages of MWCNTs and other variable parameters according to the design obtained from the Design of Expert (DOE). The parameters used for this research is as shown in Table 1. The initial pH of the stock solution was adjusted by using 1.0 M of NaOH by adding in a few drops of the alkaline solution in the 100 mL of 10 mg/L of Cd(II) until the desired pH was obtained. The MWCNTs were then added into the 100 mL of 10 mg/L of Cd(II) solutions and it was agitated according to the parameters displayed in Table 1. At the end of each interval of the time, the suspensions were shaken and centrifuged at 4000 rpm for 10 min and the supernatant was withdrawn and filtered by using qualitative filter paper having a pore size of 3 μm. The filtrates were analyzed for contaminants by ICP-OES (PerkinElmer 7000 DV) in an air-argon flame using PerkinElmer multimetal standard solutions. By ICP-OES, the metals in water sample can be analysed. It detects the concentration of Cd(II) in ppm level in the solution and volume of sample required is only 1 mL for one analysis. The experimental errors of ICP-OES were within the range of ±2.461% to ±2.983%. The Cd(II) residual concentrations were measured from the standard calibration

Table 1
Experimental design for batch adsorption.

Factor	Name	Units	Low	High	Low coded	High coded
1	pH		4	6	-1	1
2	CNTs dosage	g	0.05	0.15	-1	1
3	Agitation Speed	rpm	120	200	-1	1
4	Contact Time	min	20	80	-1	1

curve. All the data presented are the average of three replicates. Differences between the initial and the equilibrium metal ion concentrations determine the amount of metal ions being adsorbed. The adsorption capacity of MWCNTs at a specific time, t as for the adsorption kinetic study were calculated by using Eq. (1) while the adsorption equilibrium for Cd(II) was determined by Eq. (2).

$$q_t (\text{mg/g}) = \frac{(C_0 - C_t)V}{m} \quad (1)$$

$$q_e (\text{mg/g}) = \frac{(C_0 - C_e)V}{m} \quad (2)$$

where C_0 represent the initial concentration of Cd(II) solution (mg/L), q_t represents the concentration of Cd(II) at time t (mg/g), C_e represents the equilibrium concentration of Cd(II) (mg/L) respectively, V represents the volume of Cd(II) stock solution (L) and m indicates the weight of the adsorbent used (g).

Adsorption isotherms were studied by adding 0.1 g of the adsorbents into 100 mL solution with initial pH values of 5.0 and Cd(II) concentrations from 10 to 80 mg/L. After the suspensions were shaken for 2 h, the Cd(II) concentration in the solution was measured and the amount of Cd(II) adsorbed at equilibrium was calculated using the above Eqs. (1) and (2).

Characterization of MWCNTs

The physical structure and morphology of the MWCNTs had been examined by the field emission scanning electron microscope (FESEM). All pH measurements were carried out using Mettler

Toledo type (MP220 model, USA). The heavy metal ion concentrations were measured by Inductively Couple Plasma (ICP) at 228.802 nm Cd(II).

Results and discussion

Characterization MWCNTs with and without adsorption of Cd(II)

Fig. 1(a)–(d) represents the characterization of optimum MWCNTs produced using microwave heating before and after adsorption of Cd(II) which was examined by Field Emission Scanning Electron Microscopy (FESEM) (Zeiss, Auriga). Fig. 1(a) and (b) FESEM images at different magnifications, i.e. 1000 and 1000,000 nm scales. These produced CNT is free from impurity was observed from all the images and clear MWCNTs was observed. It also shows that these MWCNT are tens of microns long with uniform diameters. The bulk morphology of long MWCNT is filmed like and oriented. The produced MWCNTs have the vertical alignment of CNT could be observed with the diameter of CNTs ranging from 13 to 20 nm. These images indicate that despite the long growth time and centimetre length, the tubes grew vertically without any interruption until the catalyst activity was terminated. The uniform diameter of CNTs shows that MWCNTs produced were in homogenized form. These results are in good agreement with previous researchers [24–26]. On the other hand, Fig. 1(c) and (d) represents the characterization for after adsorption of Cd(II) with a different magnification of 1000 and 1,000,000 nm scale. In general, after the adsorption process tube was swill from an open end of the MWCNTs tube where functional groups such as hydroxyl or carboxyl groups which were formed

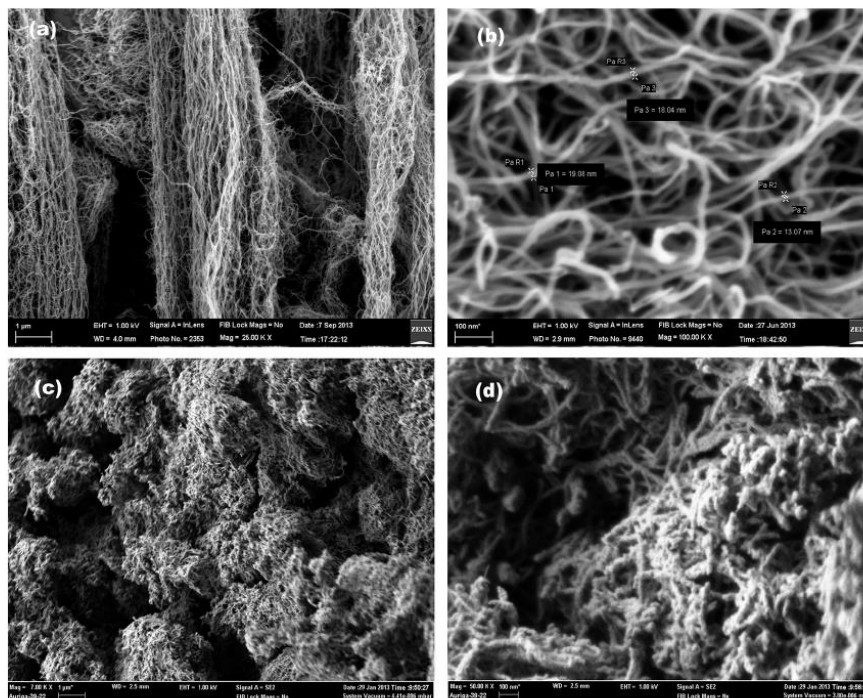


Fig. 1. FESEM images of optimum MWCNTs produced (a and b) before and (c and d) after adsorption.

through the adsorption process will attach to it or to any other available defect sites [27]. Hence, the surface of MWCNTs after adsorption will be less smooth than before adsorption MWCNTs due to the modification of MWCNTs surface after adsorption [28,29].

FTIR analysis of Cd(II) adsorption

The surface chemistry in terms of functional group which is adhered to the surface of MWCNTs during the adsorption of Cd(II) process can be classified by employing Fourier Transform Infrared (FTIR) spectroscopy (Bruker, IFS66 v/S). As for this research, FTIR was engaged as well to determine the functional groups attached on the before and after adsorption of Cd(II). Microwave assisted synthesis of MWCNTs having a high BET surface area with high quality of CNTs produced were reported in previous study [23]. Adsorption behaviour of any adsorbent is influenced by the chemical reactivity of the surface especially when the chemically bonded oxygen exists on it various forms of functional groups [30,31]. The rule of surface functionalities increase significantly relative to the pore size distribution of BET surface area, and in many cases dominates [32]. Hence, microwave assisted synthesis of MWCNTs have a some functional group present on the surface of MWCNTs. In this study have achieved and outstanding adsorption capacity was achieved compared to modified CNTs which was reported in previous study [33–35]. Fig. 2(a) and (b) demonstrates the plot for optimized condition of MWCNTs before and after adsorption of Cd(II). Fig. 2(a) The peaks observed on before MWCNTs adsorption at a range of 1700–1900 cm^{-1} defines the carboxylic group, followed by aromatic C=C groups at 1450–1600 cm^{-1} and O–H groups at 2800–3000 cm^{-1} as well. This observation was observed as grown MWCNTs, a very small amount of oxygen group present on the surface of MWCNTs due to synthesis condition to enhance high quality and high purity of MWCNT. Fig. 2(b) shows after adsorption of Cd(II), it was observed several peaks were observed. The C=O and C–O is stretching frequencies shifted from 1705 and 1200 cm^{-1} . Peaks at 1600 cm^{-1} of amino-functionalized MWCNTs are due to the N–H stretching of amine groups. Peaks at 2930 and 2860 cm^{-1} are greatly enhanced because of the attachment of additional methyl groups. Peaks between 950 and 700 cm^{-1} are due to the stretching mode of aromatic amine groups, and peaks at 2370 cm^{-1} may be because of the existence of ammonium ions [36–38]. After adsorption of Cd(II) process would create an open end to the MWCNTs where additional functional groups such as carboxylic group would

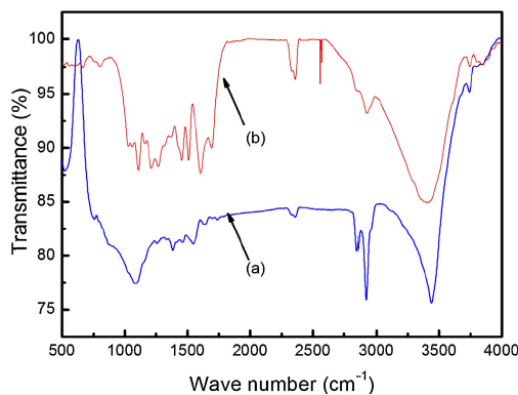


Fig. 2. FTIR adsorption spectra for (a) MWCNTs before (b) MWCNTs after adsorption of Cd(II).

attach to it or any available defect sites [6,39]. The hydrophilic surface structure provides the functionalized MWCNTs an advantage of high dispersion in water, which eventually leads to a higher adsorption capacity of Cd(II) ions from aqueous solution compared with before the adsorption of MWCNTs. This finding corresponds to many results reported by several previous researchers who studied on the surface chemistry of CNTs [36–38,40–42].

Thermogravimetric analysis of MWCNTs

The variations of the MWCNTs mass with respect to temperatures at specific time were revealed in Fig. 3. A single peak at one distinct zone, implying high purity of the MWCNTs was shown in TGA analysis. Since no other peaks are observed, so the peak corresponds to the decomposition of one element only. The weight between 50 and 100 °C which correspond to the loss of water from the catalyst support was a very minor loss. In the range of 335–350 °C of weight loss is effected of oxidation of amorphous carbon [43–45] and the weight loss in the range of 480–620 °C is due to oxidation of MWCNTs [44]. The metal catalyst and support are not volatile below 800 °C and thus remain as residue of TGA was revealed in the observed flat profiles between 620 and 850 °C. The purity and yield of MWCNTs was shown by the weight loss and as the higher the weight loss, as the higher is the purity of MWCNTs. Hence, after sorbent adsorption of Cd(II) clearly confirm the stability of MWCNTs. The previous research [23,46,47] was verified by the above finding.

Statistical optimization of removal of Cd(II) using MWCNTs

In order to determine the most suitable adsorbent with the highest adsorption capacity of Cd(II) from aqueous solutions, the first crucial step would be to determine the optimized condition of MWCNTs as a the adsorbent for removal of Cd(II). Specific runs for the optimized condition were conducted based on the design obtained from the (DOE). The results obtained from this particular experiment were analysed using the application of “analysis of variance” (ANOVA) obtained from the DOE and the optimized variables are attainable from Table 1. The analyses obtained by the application of ANOVA for the removal of Cd(II) using MWCNTs are indicated in Table 2. From the values obtained in Table 2, the fisher F-test value can be related to the mean square of the regressed model which leads to the comparative mean square of the residuals (errors). The F value proves the efficiency of the model as its value increases. On the other hand, low probability, P value indicates higher significance of the regression model. Hence, from Table 2, it can be seen that the F-test values using MWCNTs were 19, which indicates that the model are significant. Besides that, the

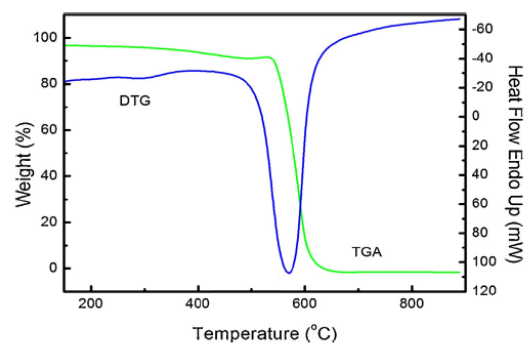


Fig. 3. TGA analysis of the MWCNTs after sorbent adsorption of Cd(II).

Table 2
ANOVA for the selected factorial Model for removal of Cd(II).

Source	Sum of squares	DF	Mean square	F Value	Prob > F	Status	
Model	6118.869	14	437.062	19.0	<0.0001	Significant	
A	6.7222	1	6.7222	0.3	0.5994		
B	41.405	1	41.405	1.8	0.2066		
C	1.2272	1	1.22722	0.1	0.8215		
D	55.827	1	55.827	2.4	0.1474		
A ²	265.673	1	265.673	11.6	0.0059		
B ²	389.673	1	389.673	17.0	0.0017		
C ²	102.785	1	102.785	4.5	0.0581		
D ²	199.913	1	199.913	8.7	0.0132		
AB	24.2556	1	24.2556	1.1	0.3263		
AC	130.530	1	130.530	5.7	0.0363		
AD	1.15562	1	1.15562	0.1	0.8267		
BC	1.15562	1	1.15562	0.1	0.8267		
BD	57.3806	1	57.3806	2.5	0.1424		
CD	24.255	1	24.255	1.1	0.3263		
Residual	252.789	11	22.980				Non-significant
Lack of Fit	252.28	10	25.228	50.5	0.1092		
Pure Error	0.5	1	0.5				
Cor Total	6371.658	25					

values of the correlation coefficient, *R*-squared and Adj *R*-squared for MWCNTs were 0.96 and 0.90 respectively. This value implies that the model of the adsorbent is very close to each other, which indicates the high efficiency and significance of the model. The model equation evolved for the removal of Cd(II) from aqueous solutions for MWCNTs (3) are as follows:

$$\begin{aligned} \text{Cd(II) Removal (\%)} = & 96.50 + 0.61 \times A - 1.52 \times B - 0.26 \\ & \times C + 1.76 \times D - 10.19 \times A^2 - 12.34 \\ & \times B^2 - 6.34 \times C^2 - 8.84 \times D^2 - 1.23 \\ & \times A \times B + 2.86 \times A \times C + 0.27 \times A \times D \\ & - 0.27 \times B \times C + 1.89 \times B \times D + 1.23 \\ & \times C \times D \end{aligned} \quad (3)$$

Consequently, variables *A*, *B*, *C*, *D*, *AB*, *AC*, *AD*, *BC*, *BD*, and *CD* were significant model terms. This indicates that the pH (*A*), agitation speed (*B*), MWCNTs dosage (*C*) and time (*D*) were highly significant values of Probe >*F* was 0.001. The coefficient of single factor represents the effect of its represented factor while the coefficients of double factors represent the interaction and effect of both represented factor. Hence, following up to the equation, the positive sign in the equation represents the synergistic effect while the negative sign represents antagonistic effect values. Fig. 4 shows theoretical values versus the experimental values for Cd(II)

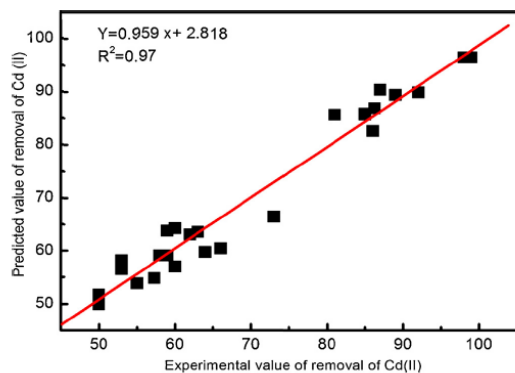


Fig. 4. Relationship between actual value vs. predicted values of removal of Cd(II).

removal. It was clearly shown that the theoretical values obtained were quite close to experimental values, indicating that the model developed was successful in bridging the correlation between process parameters for removal of Cd(II).

Fig. 5 represents the 3-dimensional (3-D) plot for adsorption of Cd(II) on MWCNTs affected by pH, MWCNTs dosage and agitation speed. The 3-D plot of the interaction between agitation speed and pH are as depicted in Fig. 5(a) which shows that as pH increases with the increasing of agitation speed, removal of Cd(II) obtained the highest at pH 5 an 160 rpm agitation speed gave maximum removal of Cd(II). Further increase in pH and agitation speed resulted in decreased Cd(II) removal. This is due to the effects of precipitation of Cd(II) at relatively high values of pH (alkaline condition). The value of pH of the aqueous solution plays a major role in the adsorption of heavy metals [1,10,11] Fig. 5(b) shows the interaction between pH and MWCNTs dosage where it was observed that removal of Cd(II) reached to the maximum when the pH and MWCNTs dosage is at its centre point. Further increased in pH and MWCNTs dosage resulted in Cd(II) adsorption decreased. From the observation, increased in MWCNTs dosage from 0.05 to 0.1 increase the removal of Cd(II) linearly. Furthermore, the increase in the adsorbed amount leads to increase in active sites concentration which helps in adjusting the adsorption solution electrostatic charge to an adsorption preferable level by removing the competitive H⁺ ions [10,48]. On the other hand, the adsorption capacity is highly dependent on the pH where H₂O₂ oxidizes the MWCNTs to reach an equilibrium state with a high adsorption capacity at lower pH [10]. Fig. 5(c) shows the interaction between time and pH. The elliptical plot indicated that there is good interaction between time and pH. The mid-point interaction for a time and pH shows the highest removal of Cd(II) obtained. Further increase in time 35–60 min and pH 5 to 6 resulted in decreased of Cd(II) removal [49].

Adsorption isotherm

Adsorption isotherm reflects the relationship between the amount of a solute adsorbed at constant temperature and its concentration in the equilibrium solution. It provides essential physicochemical data for assessing the applicability of the adsorption process as a complete unit operation. The successful representation of the dynamic adaptive separation of solute from solution onto an adsorbent depends upon a good description of the equilibrium separation between the two phases [9,12,50–52]. The relation between contact time (min) versus adsorption capacity

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